

Two-Degree-of-Freedom Controller Design for an Ill-Conditioned Distillation Process Using μ -Synthesis

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Abstract—The structured singular value framework is applied to a distillation benchmark problem formulated for the 1991 IEEE Conference on decision and control (CDC). A two degree of freedom controller, which satisfies all control objectives of the CDC problem, is designed using μ -synthesis. The design methodology is presented and special attention is paid to the approximation of given control objectives into frequency domain weights.

Index Terms— H -infinity control, process control, robustness, structured singular value, uncertainty.

I. INTRODUCTION

THE PURPOSE OF THIS paper is to demonstrate, by way of an example, how the structured singular value (SSV, μ) framework [4] may be used to design a robust controller for a given control problem. The problem involves an uncertain system and control objectives that cannot be directly incorporated into the μ -framework. In particular, we consider how to approximate the given problem as a μ -problem by deriving suitable frequency dependent weights. These define the model uncertainty and control objectives in the μ -framework.

The control problem studied in this paper was introduced by Limebeer [9] as a benchmark problem at the 1991 Conference on Decision and Control (CDC), where it formed the basis for a design case study aimed at investigating the advantages and disadvantages of various controller design methods for ill-conditioned systems.

The problem originates from Skogestad *et al.* [18] where a simple model of a high purity distillation column was used to demonstrate that ill-conditioned plants are potentially extremely sensitive to model uncertainty. In [18] uncertainty and performance specifications were given as frequency dependent weights, i.e., the problem was *defined* to suit the μ -framework and therefore a μ -optimal controller yields the optimal solution to that problem.

However, in the CDC benchmark problem [9] uncertainty is defined in terms of parametric gain and delay uncertainty and the control objectives are a mixture of time domain and

frequency domain specifications. These specifications cannot be directly transformed into frequency dependent weights, but have to be approximated to fit into the μ -framework.

The distillation problem in [18] and variants of this problem, like the CDC problem [9], has been studied by several authors, e.g., Freudenberg [6], Yaniv and Barlev [22], Lundström *et al.* [11], Hoyle *et al.* [7], Postlethwaite *et al.* [15], Yaniv and Horowitz [23] and Zhou and Kimura [25]. In three recent studies; Limebeer *et al.* [10], van Diggelen and Glover [3] and Whidborne *et al.* [21], two degree of freedom controllers are designed for the CDC problem. The three latter papers are all based on the loop shaping design procedure of McFarlane and Glover [14], where uncertainties are modeled as \mathcal{H}_∞ -bounded perturbations in the normalized coprime factors of the plant. To obtain the desired performance, [10] use a reference model design approach, [3] use the Hadamard weighted \mathcal{H}_∞ -Frobenius formulation from [2], while [21] use the method of inequalities [24] where the performance requirements are explicitly expressed as a set of algebraic inequalities.

The two degree of freedom design in this paper differs from [10], [3], and [21] in that we use μ -synthesis for our design. With this method uncertainty is modeled as linear fractional uncertainty and performance is specified as in a standard \mathcal{H}_∞ -control problem. Like [10], we specify some of the control objectives as a model-matching problem.

This paper is organized as follows: A brief introduction to the μ -framework is presented in Section II. The benchmark problem is defined in Section III. In Section IV we outline the design method used in this paper. In Section V we gradually transform (approximate) the given problem into a μ -problem and demonstrate the effect of different weight adjustments. The final controller designed in this section demonstrates that the control objectives defined by Limebeer [9] are achievable. Finally the results are discussed and summarized.

All of the results and simulations presented in this paper were computed using the MATLAB “ μ -Analysis and Synthesis Toolbox” [1].

II. CDC PROBLEM DEFINITION

The plant model and design specifications for the CDC benchmark problem [9] are presented in this section.

A. Plant Model

The process to be controlled is a distillation column with reflux flow and boilup flow as manipulated inputs and product compositions as outputs. The resulting model

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is ill-conditioned, as is here given by

$$\hat{G}(s) = \frac{1}{75s+1} \begin{bmatrix} 0.878 & -0.864 \\ 1.082 & -1.096 \end{bmatrix} \begin{bmatrix} k_1 e^{-\theta_1 s} & 0 \\ 0 & k_2 e^{-\theta_2 s} \end{bmatrix} \quad (1)$$

$$k_i \in [0.8 \ 1.2]; \quad \theta_i \in [0.0 \ 1.0]. \quad (2)$$

In physical terms this is equivalent to a gain uncertainty of $\pm 20\%$ and a delay of up to 1 min in each input channel. The set of possible plants defined by (1)–(2) is denoted Π in the sequel.

B. Design Specifications

Specifications **S1** to **S4** should be fulfilled for *every* plant $\hat{G} \in \Pi$:

S1 Closed-loop stability.

S2 For a unit step demand in channel 1 at $t = 0$ the plant outputs y_1 (tracking) and y_2 (interaction) should satisfy:

- $y_1(t) \geq 0.9$ for all $t \geq 30$ min;
- $y_1(t) \leq 1.1$ for all t ;
- $0.99 \leq y_1(\infty) \leq 1.01$;
- $y_2(t) \leq 0.5$ for all t ;
- $-0.01 \leq y_2(\infty) \leq 0.01$.

Corresponding requirements hold for a unit step demand in channel 2.

S3 $\bar{\sigma}(K_y \hat{S}) < 316$, $\forall \omega$. This specification is mainly added to avoid saturation of the plant inputs.

S4 Alt.1: $\bar{\sigma}(\hat{G} K_y) < 1$ for $\omega \geq 150$.

S4 Alt.2: $\bar{\sigma}(K_y \hat{S}) < 1$ for $\omega \geq 150$.

Here K_y denotes the feedback part of the controller and $\hat{S} = (I + \hat{G} K_y)^{-1}$ the sensitivity function for the worst case \hat{G} .

Specifications **S3** and **S4** are not explicitly stated in [9], but formulated as “the closed-loop transfer function between output disturbance and plant input $[K_y \hat{S}]$ be gain limited to about 50 dB [≈ 316 (**S3**)] and the unity gain cross over frequency of the largest singular value should be below 150 rad/min [**S4**].” Different researchers have given the latter specification different interpretations, e.g., [3] use Alt.1. while [21] use Alt.2. For the purpose of this paper, this diversity is advantageous, since it gives us the opportunity to start with the easier alternative (Alt.1) and then show how to refine the μ -problem to achieve the tougher requirement (Alt.2).

In practice, specification **S4** Alt.1 is implied by **S1**, so the actual performance requirements are **S2** and **S3** (and **S4** Alt.2).

Most of the specifications in this paper may be viewed as bounds on transfer functions from some inputs to some outputs. The notation for these transfer functions is defined by Fig. 1 and the matrices in (4)–(5). The controller K in Fig. 1 may be a one degree of freedom controller (ODF) or a two degree of freedom controller (TDF). A TDF controller may be partitioned into two parts

$$K = [K_r \ K_y] = \begin{bmatrix} A_K & B_{K_r} & B_{K_y} \\ C_K & D_{K_r} & D_{K_y} \end{bmatrix} \quad (3)$$

where K_y is the feedback part of the controller and K_r is the prefilter part.

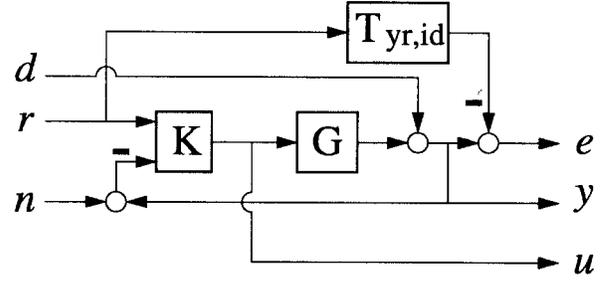


Fig. 1. Block diagram without weight functions.

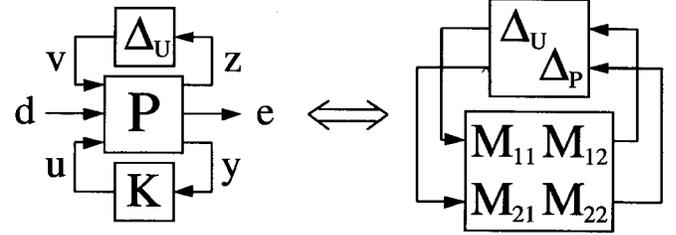


Fig. 2. General problem description.

For an ODF controller $K_r = K_y$, which yields the following transfer functions:

$$\begin{bmatrix} e \\ y \\ u \end{bmatrix} = \begin{bmatrix} S & T - T_{yr,id} & -T \\ S & T & -T \\ -K_y S & K_y S & -K_y S \end{bmatrix} \begin{bmatrix} d \\ r \\ n \end{bmatrix} \quad (4)$$

where $S = (I + G K_y)^{-1}$ is the sensitivity function, $T = (I + G K_y)^{-1} G K_y$ is the complementary sensitivity function and $T_{yr,id}$ is the reference model for the setpoint change. Note that if $T_{yr,id} = I$, then the transfer function from r to e is $T - T_{yr,id} = -S$.

For a TDF controller $K_r \neq K_y$, which yields the following transfer functions:

$$\begin{bmatrix} e \\ y \\ u \end{bmatrix} = \begin{bmatrix} S & S G K_r - T_{yr,id} & -T \\ S & S G K_r & -T \\ -K_y S & (I + K_y G)^{-1} K_r & -K_y S \end{bmatrix} \begin{bmatrix} d \\ r \\ n \end{bmatrix}. \quad (5)$$

In this case, the transfer function from r to e is not equal to $-S$ if $T_{yr,id} = I$.

III. THE μ -FRAMEWORK

This section gives a very brief introduction to μ -analysis and synthesis and defines some of the nomenclature used in the rest of the paper. For further details, the interested reader may consult for example [18], [19] and [1].

The \mathcal{H}_∞ -norm of a transfer function $M(s)$ is the peak value of the maximum singular value over all frequencies

$$\|M(s)\|_\infty \equiv \sup_\omega \bar{\sigma}(M(j\omega)). \quad (6)$$

The left block diagram in Fig. 2 shows the general problem formulation in the μ -framework. It consists of an augmented plant P (including a nominal model and weighting functions), a controller K and a (block-diagonal) perturbation matrix $\Delta_U = \text{diag}\{\Delta_1, \dots, \Delta_n\}$ representing the uncertainty.

Uncertainties are modeled by the perturbations (Δ_i 's) and uncertainty weights included in P . These weights are chosen such that $\|\Delta_U\|_\infty \leq 1$ generates the family of all possible plants to be considered. In principle Δ_U may contain both real and complex perturbations, but in this paper only complex perturbations are used.

The performance is specified by weights in P which normalize \mathbf{d} and \mathbf{e} such that a closed-loop \mathcal{H}_∞ -norm from \mathbf{d} to \mathbf{e} of less than 1 (for the worst case Δ_U) means that the control objectives are achieved.¹

The framework in Fig. 2 may be used for both one degree of freedom (ODF) and two-degree-of-freedom (TDF) controller design. In the ODF case the controller input \mathbf{y} is the difference between set-points and measured plant outputs, $\mathbf{y} = r - y_m$, while in the TDF case $\mathbf{y} = [r^T \ -y_m^T]^T$.

The right block diagram in Fig. 2 is used for robustness analysis. M is a function of P and K , and Δ_P ($\|\Delta_P\|_\infty \leq 1$) is a fictitious ‘‘performance perturbation’’ connecting \mathbf{e} to \mathbf{d} . Provided that the closed-loop system is nominally stable the condition for robust performance (RP) is

$$\text{RP} \Leftrightarrow \mu_{\text{RP}} = \sup_{\omega} \mu_{\Delta}(M(j\omega)) < 1 \quad (7)$$

where $\Delta = \text{diag}\{\Delta_U, \Delta_P\}$.

μ is computed frequency-by-frequency through upper and lower bounds. Here we only consider the upper bound

$$\mu_{\Delta}(M(j\omega)) \leq \inf_{D \in \mathbf{D}} \bar{\sigma}(DMD^{-1}) \quad (8)$$

where $\mathbf{D} = \{D \mid D\Delta = \Delta D\}$.

At present there is no direct method to synthesize a μ -optimal controller, however, μ -synthesis (DK-iteration) which combines μ -analysis and \mathcal{H}_∞ -synthesis often yields good results. This iterative procedure was first proposed in [5] and [16]. The idea is to attempt to solve

$$\min_K \inf_{D \in \mathbf{D}} \sup_{\omega} \bar{\sigma}(DMD^{-1}) \quad (9)$$

(where M is a function of K) by alternating between minimizing $\sup_{\omega} \bar{\sigma}(DMD^{-1})$ for either K or D while holding the other fixed. The iteration steps are as follows.

- DK1** Scale the interconnection matrix M with a stable and minimum phase rational transfer matrix $D(s)$ with appropriate structure (an identity matrix with right dimensions is a common initial choice).
- DK2** Synthesize an \mathcal{H}_∞ -controller for the scaled problem, $\min_K \sup_{\omega} \bar{\sigma}(DMD^{-1})$.
- DK3** Stop iterating if the performance is satisfactory or if the \mathcal{H}_∞ -norm does not decrease, else continue.
- DK4** Compute the upper bound on μ (8) to obtain new D -scales as a function of frequency $D(j\omega)$.
- DK5** Fit the magnitude of each element of $D(j\omega)$ to a stable and minimum phase rational transfer function and go to **DK1**.

Each of the minimizations (steps **DK2** and **DK4**) are convex, but joint convexity is not guaranteed.

The \mathcal{H}_∞ -controller synthesized in step **DK2** has the same number of states as the augmented plant P plus twice the number of states of D , hence it is desirable to keep the order of P and the D -scales as low as possible whilst satisfying the controller specification criteria.

IV. DESIGN PROCEDURE

The CDC specifications in Section II cannot be directly applied in the μ -framework. The reasons for this are: 1) The gain-delay uncertainty in (1)–(2) has to be approximated into linear fractional uncertainty (Fig. 2); 2) Specification **S2** needs to be approximated since it is defined in the time domain; 3) In the μ -framework, it is not possible to directly bound the four SISO transfer functions associated with **S2** and the 2×2 transfer function associated with **S3** (and **S4 Alt.2**). Instead these control objectives must be reflected in the \mathcal{H}_∞ -norm of the transfer function from \mathbf{d} to \mathbf{e} (Fig. 2).

The following approach makes it possible to apply μ -synthesis to this kind of problem.

- 1 Approximate the given problem into a μ -problem.
- 2 Synthesize a robust controller for the μ -problem.
- 3 Verify that the controller satisfies the original specifications (**S1–S4**) for the original set of plants (**II**).

Step 1 is our major concern in this paper. Several approaches may be used to obtain the μ -problem, however, the following are general guidelines: 1) Choose \mathbf{d} and \mathbf{e} such that all essential control objectives are reflected in the \mathcal{H}_∞ -norm of the transfer function between these signals. At the same time keep the dimension of \mathbf{d} and \mathbf{e} as small as possible. 2) Use low-order uncertainty and performance weights to keep the order of P and thereby the order of the controller low. The complexity and order of these weights may be increased later, if required. 3) Use weighting parameters with physical meaning, since these parameters are the ‘‘tuning knobs’’ during the design stage. The derivation of such weighting functions for the CDC problem is treated in detail in the next section.

Step 2 is fairly straightforward using DK-iteration and the available software (e.g., [1]). Experience with this iterative scheme shows that, for the first few iterations, it is best if the controller synthesized in step **DK2** is slightly suboptimal (\mathcal{H}_∞ -norm 5–10% larger than the optimal) and that the D -scale fit in step **DK5** is of low order. In subsequent iterations, controllers that are close to optimality and higher order D -scales may be used if required. However, it is also recommended that the final controller is slightly suboptimal since this yields a blend of \mathcal{H}_∞ and \mathcal{H}_2 optimality with generally better high frequency roll-off than the optimal \mathcal{H}_∞ -controller.

Step 3 is, in this paper, performed using time simulations with the four extreme combinations of gain uncertainty (2) and a 1 min delay (approximated as a second-order Padé approximation).

V. CONTROLLER DESIGN

In this section we design controllers for the benchmark problem, using the design procedure outlined above. Actually,

¹Note that \mathbf{d} and \mathbf{e} in Fig. 2 are not equivalent to d and e in Fig. 1, but may contain d and e among other signals.

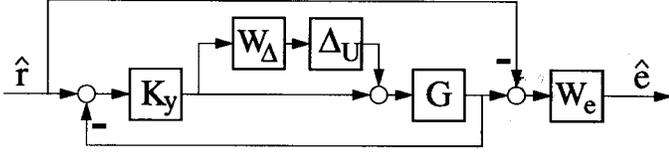


Fig. 3. Original ODF-problem formulation.

we start with a controller designed for the “original” problem defined in Skogestad *et al.* [18] and check the performance of this controller with respect to the CDC specifications defined in Section II. We then gradually refine the μ -formulation by adding further input and output signals to \mathbf{d} and \mathbf{e} and by adjusting the uncertainty and performance weighting functions.

This gradual approach clearly demonstrates the effect of the weighting function refinements, and thereby is of tutorial value. Moreover, it is also a good approach for “real” problems, since one should not put more effort into the μ -formulation than required, that is, one should start with a simple problem formulation, and refine the problem formulation if the specifications are not met.

A. ODF-Controller for “Original” Specifications

The “original” problem presented in [18] is defined in the frequency domain in terms of Fig. 3 and the following transfer function matrices:

$$G(s) = \frac{1}{75s + 1} \begin{bmatrix} 0.878 & -0.864 \\ 1.082 & -1.096 \end{bmatrix} \quad (10)$$

$$W_{\Delta}(s) = \frac{(s + 0.2)}{(0.5s + 1)} I_{2 \times 2} \quad (11)$$

$$W_e(s) = \frac{1}{2} \frac{(20s + 2)}{20s} I_{2 \times 2} \quad (12)$$

$$\Delta_U(s) = \text{diag}\{\Delta_1, \Delta_2\}; \quad \|\Delta_U(s)\|_{\infty} \leq 1. \quad (13)$$

Remark: As shown in [12], the uncertainty weight in (11) does not quite cover (include) the gain and delay uncertainty defined in Section II; the allowed time delay is about 0.9 min rather than 1 min, and the magnitude of the weight approaches 2.0 at high frequencies rather than 2.2.

The resulting μ -synthesis problem is then

$$\min_K \mu_{\Delta}(N); \quad N = \begin{pmatrix} W_{\Delta} K S G & W_{\Delta} K S \\ W_e S G & W_e S \end{pmatrix} \quad (14)$$

$$\Delta = \text{diag}\{\Delta_U, \Delta_P\}.$$

Skogestad *et al.* (1988) [18] used DK-iteration with some early \mathcal{H}_{∞} -software to design a controller with six states giving a value of $\mu = 1.067$. Lundström *et al.* [11] assumed full block uncertainty Δ_U (for numerical convenience) and used the state-space \mathcal{H}_{∞} -software to obtain a μ -optimal controller with 22 states and $\mu = 0.978$. In the following we use a slightly improved controller with 18 states and $\mu = 0.9735$. This controller may be synthesized using \mathcal{H}_{∞} -synthesis and the following D -scales:

$$D(s) = \text{diag}\{d(s), d(s), I_{2 \times 2}\} \quad (15)$$

TABLE I
CONTROL PERFORMANCE FOR ODF-ORIGINAL WITH GAIN UNCERTAINTY AND A SECOND-ORDER PADÉ APPROXIMATION OF A 1-MIN DELAY. (SEE ALSO FIG. 4)

step ch.	gain unc.		set-point tracking			interaction	
	k_1	k_2	$t = 30$	max	$t = 100$	max	$t = 100$
1	1.2	1.2	0.989	1.008	1.000	0.856	0.000
1	1.2	0.8	0.934	1.001	1.001	1.047	0.000
1	0.8	1.2	0.941	1.006	1.000	0.427	-0.001
1	0.8	0.8	0.889	1.000	1.000	0.625	0.000
2	1.2	1.2	0.993	1.095	1.000	0.859	0.001
2	1.2	0.8	0.964	1.007	1.000	0.536	-0.001
2	0.8	1.2	0.956	1.198	1.001	0.934	0.000
2	0.8	0.8	0.929	1.000	1.000	0.627	0.000

TABLE II
CONTROL PERFORMANCE FOR TDF-ORIGINAL WITH GAIN UNCERTAINTY AND A SECOND-ORDER PADÉ APPROXIMATION OF A 1-MIN DELAY. (SEE ALSO FIG. 7)

step ch.	gain unc.		set-point tracking			interaction	
	k_1	k_2	$t = 30$	max	$t = 100$	max	$t = 100$
1	1.2	1.2	0.889	1.008	1.003	0.175	0.004
1	1.2	0.8	0.913	1.000	1.000	0.497	0.000
1	0.8	1.2	0.902	1.000	1.000	0.257	0.000
1	0.8	0.8	0.905	1.000	1.000	0.156	0.000
2	1.2	1.2	0.891	1.014	1.005	0.175	0.004
2	1.2	0.8	0.917	1.000	1.000	0.126	0.000
2	0.8	1.2	0.928	1.000	1.000	0.368	0.000
2	0.8	0.8	0.921	1.000	1.000	0.156	0.000

where

$$d(s) = 2.0 * 10^{-5} \times \frac{(s + 1000)(s + 0.25)(s + 0.054)}{(s + 0.67 + j0.56)(s + 0.67 - j0.56)(s + 0.013)}. \quad (16)$$

We denote this controller “ODF-original.” In fact, it can be shown [8] that the resulting controller has the form of a SVD-controller $K(s) = V\tilde{K}(s)U^T$ where $\tilde{K}(s)$ is diagonal and V and U are the input and output singular vector matrices for the plant $G(s)$, which in this case are real and independent of frequency.

The performance of this controller applied to the CDC problem is demonstrated in Fig. 4 where time responses are shown for the four extreme uncertainty combinations defined in (1), i.e., the four gain combinations with maximum input delay. The simulation results are also summarized in Table I where bold entries mark violations on **S2**. We see that the closed-loop system is stable, ensuring that **S1** is satisfied. The setpoint tracking requirements in **S2** are almost satisfied, but the interaction is far too strong.

The performance with respect to **S3** is demonstrated in Fig. 5. It is clear that $\bar{\sigma}(K_y S)$ [the gain from setpoints r , noise n and output disturbances d to manipulated inputs u , see (4)] is far too high at high frequencies and also around the closed-loop bandwidth ($\omega \approx 0.1$ rad/min).

The performance specification in the original problem is expressed as a bound on the sensitivity function S . Fig. 6

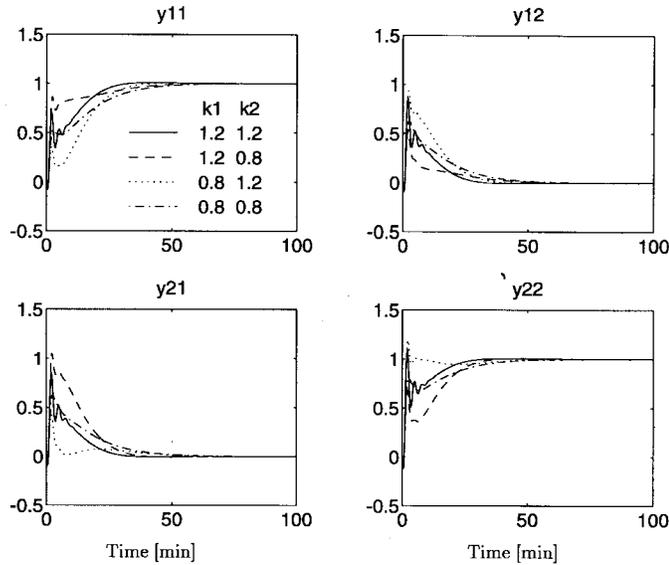


Fig. 4. Output responses for ODF-original controller with plant-model mismatch. y_{ij} shows response in output i for step change of set-point j at $t = 0$. All responses with 1 min delay (second-order Padé).

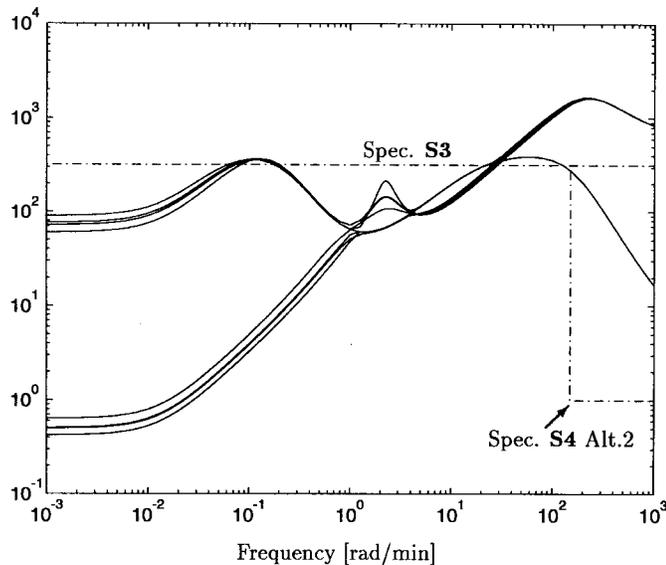


Fig. 5. Maximum and minimum singular values of $K_y \hat{S}$ for ODF-original controller for four different plants.

shows the maximum and minimum singular values of the sensitivity function for the four extreme combinations of uncertainty. From this plot we see that the original performance requirement $\bar{\sigma}(S) < |1/W_e|$ is *not* satisfied for $\omega \approx 2$ rad/min despite the fact that $\mu_{\text{RP}} < 1.0$. The explanation is that the uncertainty weight W_Δ only covers a time delay of about 0.9 min, whereas the actual delay is 1 min.

In conclusion, the one degree-of-freedom controller designed for the “original problem,” almost satisfies the tracking requirements for the CDC-problem, but the closed-loop suffers from strong interactions and excessive use of manipulated inputs, in particular at very high frequencies ($\omega > 10$ rad/min). We next see if a two degree-of-freedom (TDF) design can alleviate these problems.

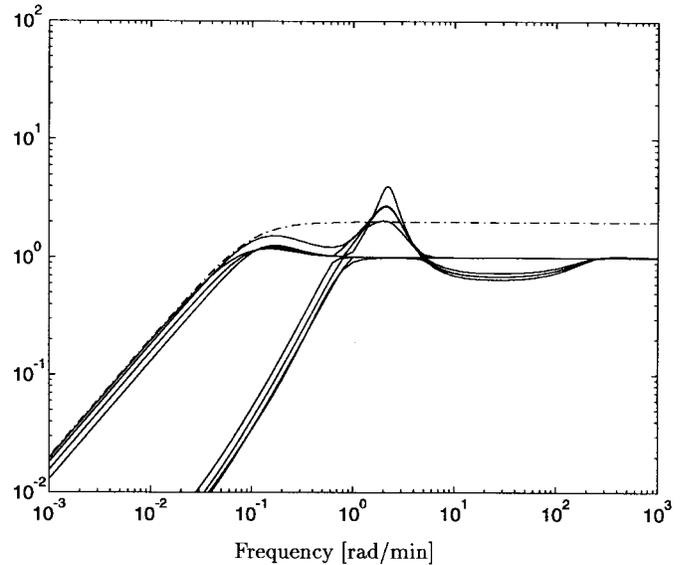


Fig. 6. Maximum and minimum singular values of \hat{S} for ODF-original controller. Dashed: Original upper bound on S [(1/ W_e), (11)].

B. TDF-Controller for “Original” Specifications

Strictly speaking, the original problem formulation of Skogestad *et al.* [18] cannot take advantage of a TDF controller, because the specification is on the sensitivity function $S = (I + GK_y)^{-1}$, which depends only on the feedback part of the controller, K_y . However, if instead, we interpret the specification in terms of the transfer function from references r to errors e , $SGK_r - I$ (see (5), with $T_{y,r,id} = I$), then robust performance can be improved by use of a TDF controller. Lundström *et al.* [11] interpreted the specifications in this way and were able to reduce μ_{RP} from 0.978 to 0.926 with a TDF controller. We denote this design “TDF-original.”

Simulations and tabulated data for the TDF-original design are shown in Fig. 7 and Table II. The setpoint tracking specification is still not quite satisfied, but the interactions have almost disappeared compared to the ODF-original response. However, there are unpleasant high-frequency oscillations in all responses. These oscillations also show up as a “ringing peak” in the closed-loop transfer functions, for example, the peak at approximately 2 rad/min in Fig. 8. This phenomena could have been eliminated if a better uncertainty weight had been used, i.e., an uncertainty weight that covers a 1 min delay (rather than only 0.9 min). More seriously, as illustrated in Fig. 8, specification **S3** with respect to input usage is not satisfied. The reason is that we have not included in the specifications any explicit penalty for input usage.

We conclude that we are not able to meet the CDC-specifications by designing a μ -optimal controller using the “original” uncertainty and performance weights. We therefore need to modify the uncertainty weight, and consider the CDC-specifications explicitly, e.g., by including a weight on $K_y S$ to satisfy **S3**.

C. Weight Selection for CDC Specifications

In this section we approximate the CDC specifications as frequency dependent weights.

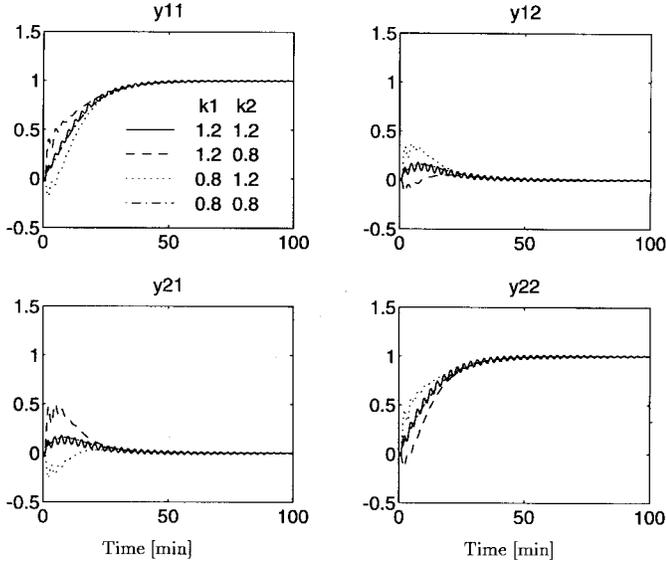


Fig. 7. Output responses for TDF-original controller with plant-model mismatch. y_{ij} shows response in output i for step change of set-point j at $t = 0$. All responses with 1-min delay (second-order Padé).

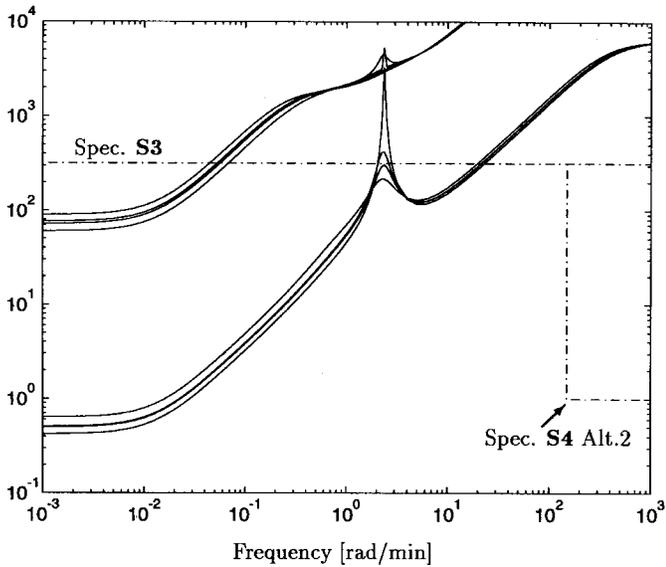


Fig. 8. Maximum and minimum singular values of $K_y \hat{S}$ for TDF-original controller for four different plants.

Uncertainty Weights: As already noted, the gain-delay uncertainty in (2) is not quite covered by the uncertainty weight defined in (11). A better weight is presented in [13]

$$W_{\Delta}(s) = \frac{(1 + \frac{k_r}{2})\theta_{\max}s + k_r}{\frac{\theta_{\max}}{2}s + 1} I_{2 \times 2} = \frac{1.1s + 0.2}{0.5s + 1} I_{2 \times 2} \quad (17)$$

where $k_r = 0.2$ is the relative gain uncertainty and $\theta_{\max} = 1$ is the maximum delay. This weight has the same low order as that of (11) and it *almost* covers the gain and delay uncertainty. A slight modification to (17) yields a weight that *completely* covers the uncertainty ([13]), but is of higher order

$$W_{\Delta}(s) = \frac{1.1s + 0.2}{0.5s + 1} \cdot \frac{(\frac{s}{2.363})^2 + 2 \cdot 0.838 \frac{s}{2.363} + 1}{(\frac{s}{2.363})^2 + 2 \cdot 0.685 \frac{s}{2.363} + 1} I_{2 \times 2}. \quad (18)$$

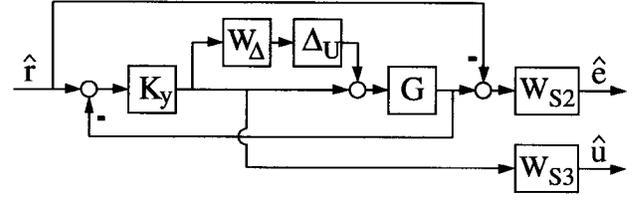


Fig. 9. Block diagram for one degree of freedom controller.

It is often fruitful to start with the simpler weight (17) and if the performance verification (Step 3 of the design procedure in Section IV) shows that this uncertainty model does not yield a robust controller for the set of plants II, then the more rigorous uncertainty model (18) should be used. This is the approach taken here.

ODF Performance Weights: A simple way to approximate the performance specifications **S2** and **S3** into a μ -problem is shown in Fig. 9, where K_y is an ODF-controller.

Here, the weight W_{S2} on the sensitivity function represents specification **S2** and weight W_{S3} represents specification **S3**. A reasonable choice for W_{S2} is the following which is taken from the original formulation:

$$W_{S2}(s) = \frac{1}{M_S} \frac{\tau_{cl}s + M_S}{\tau_{cl}s + A} I_{2 \times 2}. \quad (19)$$

For $\|W_{S2}\hat{S}\|_{\infty} < 1$ this weight yields: 1) Steady-state error less than A ; 2) Closed-loop bandwidth higher than $\omega_B = 1/\tau_{cl}$; and 3) Amplification of high-frequency output disturbances less than a factor M_S . The values used in [18] were $M_S = 2$, $A = 0$ and $\tau_{cl} = 20$.

To satisfy specification **S3** ($\|K_y\hat{S}\|_{\infty} < 316$), we choose the weight

$$W_{S3} = \frac{1}{M_{KS}} I_{2 \times 2}. \quad (20)$$

As a starting point we may choose $M_{KS} = 316$; the value given in **S3**. However, in practice this value will be too low (too tight). The reason for this is discussed in Section V-D.

In accordance with the results in Section V-A, we found that a ODF-controller did not yield the required performance; thus in the following we focus on the TDF-design.

TDF Performance Weights: For the TDF-design we use the block diagram in Fig. 10. The objective for the μ -synthesis is to minimize the worst-case weighted transfer function from references r and noise n to control error e and input signals u (the hats used in the figure indicate that the signals have been weighted). Note that the noise signal n and input signal u were not included in our μ -optimal design for the original problem, but these are needed to satisfy the CDC-specifications.

Fig. 10 gives

$$\begin{bmatrix} \hat{e} \\ \hat{u} \end{bmatrix} = \begin{bmatrix} W_e N_{11} W_r & -W_e N_{12} W_n \\ W_u N_{21} W_r & -W_u N_{22} W_n \end{bmatrix} \begin{bmatrix} \hat{r} \\ \hat{n} \end{bmatrix}. \quad (21)$$

Here

$$\begin{aligned} N_{11} &= T_{yr} - T_{yr,id} = SGK_r - T_{yr,id}; & N_{12} &= GK_y S = T \\ N_{21} &= (I + K_y G)^{-1} K_r; & N_{22} &= (I + K_y G)^{-1} K_y = K_y S \end{aligned}$$

TABLE III
FINAL WEIGHT PARAMETERS AND D -SCALES FOR DESIGN TDF-ALT.1

Weight parameters						
τ_{id}	ζ_{id}	τ_{cl}	A	M_S	M_T	M_{KS}
8.0	0.71	9.5	10^{-4}	3.5	2.0	630

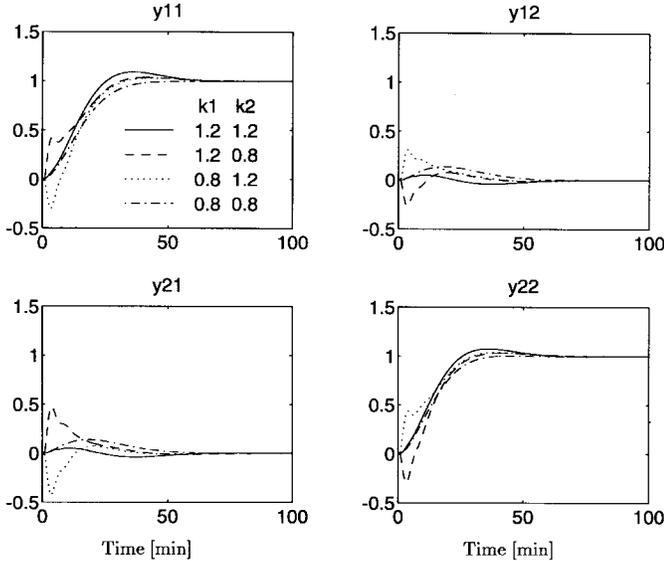


Fig. 11. Output responses for TDF-Alt.1 controller with plant-model mismatch. $y_{i,j}$ shows response in output i for step change of set-point j at $t = 0$. All responses with 1-min delay (second-order Padé).

Only two DK-iterations were needed to ensure $\mu_{RP} < 1$, however, the **S2** and **S3** performance specifications were not satisfied. M_S , M_T , and τ_{cl} were adjusted to 3.5, 2.0 and 9.5, respectively. After two more DK-iterations a controller which satisfied **S1–S4** was obtained. The controller has 24 states, yields a closed-loop \mathcal{H}_∞ -norm of 1.015 and may be synthesized using the final weights and D -scales given in Table III.

The performance of the TDF controller is demonstrated in Fig. 11 where time responses for the four extreme combinations of uncertainty are shown. The simulation results are also summarized in Table IV and are seen to satisfy specification **S2**. The maximum peak of $\bar{\sigma}(K_y \hat{S})$ is 306 (Fig. 12), which is less than 316 (50 dB), as required in **S3**, and the unit gain cross over frequency, $\bar{\sigma}(\hat{G}K_y) = 1$, is at 1 rad/min, well below 150 rad/min, as required in **S4** Alt.1. Specification **S4** Alt.2 is not satisfied as shown in Fig. 12.

The transfer functions N_{12} and N_{21} , which are not part of the CDC problem, have peak values of 3.4 and 420, respectively.

E. TDF-Controller for CDC Specifications; Alt.2

Recall that there were two alternative interpretations of specification **S4**. In this section we show that we can also satisfy specification **S4** Alt.2, which was used in [21], using the design procedure presented in this paper. We again use the problem formulation in Fig. 10, but the signal weights W_u

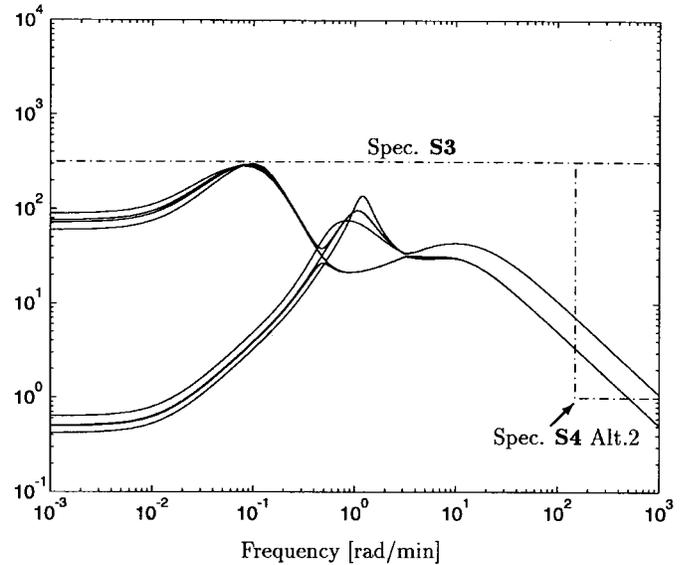


Fig. 12. Maximum and minimum singular values of $K_y \hat{S}$ for TDF-Alt.1 controller for four different plants.

TABLE IV
CONTROL PERFORMANCE FOR TDF-ALT.1 WITH GAIN UNCERTAINTY AND SECOND-ORDER PADÉ APPROXIMATION OF A 1 MIN DELAY. (SEE ALSO FIG. 11)

step ch.	gain unc.		set-point tracking			interaction	
	k_1	k_2	$t = 30$	max	$t = 100$	max	$t = 100$
1	1.2	1.2	1.066	1.092	0.998	0.051	0.001
1	1.2	0.8	0.984	1.036	0.999	0.471	-0.001
1	0.8	1.2	0.969	1.030	1.000	0.426	0.001
1	0.8	0.8	0.906	1.000	1.000	0.138	0.000
2	1.2	1.2	1.052	1.074	0.999	0.051	0.001
2	1.2	0.8	0.987	1.030	1.000	0.265	0.001
2	0.8	1.2	1.002	1.038	0.999	0.310	0.000
2	0.8	0.8	0.950	1.002	1.000	0.138	0.000

and W_n need to be modified. In addition we need to use the tighter uncertainty weight from (18).

Specifications **S3** and **S4** Alt.2 require

$$\bar{\sigma}(K_y \hat{S}(j\omega)) < \begin{cases} 50 \text{ dB} & \omega < 150 \text{ rad/min} \\ 0 \text{ dB} & \omega \geq 150 \text{ rad/min} \end{cases} \quad (28)$$

which is more difficult to satisfy than in Alt.1. We use the same procedure as in the previous design; first approximating (28) by a rational transfer function (W_{S34}), whose inverse forms an upper bound on $K_y \hat{S}$, and then deriving W_u and W_n such that $W_u W_n \approx W_{S34}$ at high frequency. Let

$$W_{S34} = \frac{1}{M_{KS}} \left(\frac{M_{KS}^{1/n} s + 1}{\frac{\omega_0}{\alpha \omega_0} s + 1} \right)^n I_{2 \times 2}. \quad (29)$$

The weight is equal to $1/M_{KS}$ at low frequencies, and then starts increasing sharply and crosses 1 at about the frequency ω_0 (which should then be about 150 rad/min). It levels off at the value c^n at high frequency. The parameter n is an integer. By increasing n , a tighter approximation of (28) is achieved,

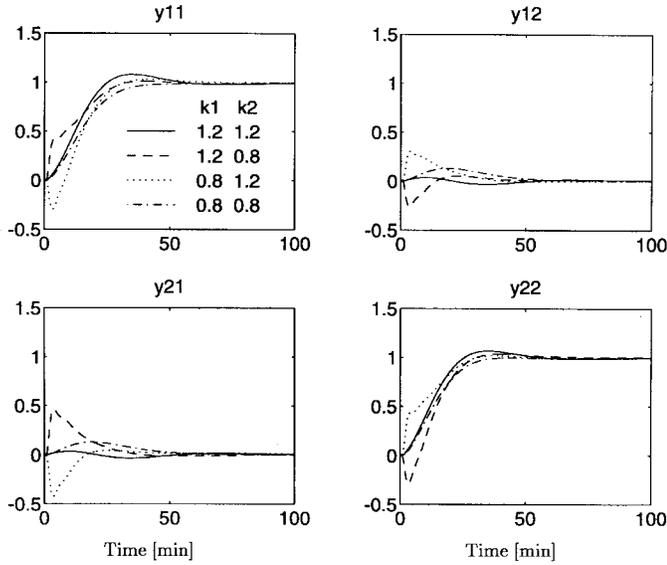


Fig. 13. Output responses for TDF-Alt.2 controller with plant-model mismatch. y_{ij} shows response in output i for step change of set-point j at $t = 0$. All responses with 1-min delay (second-order Padé).

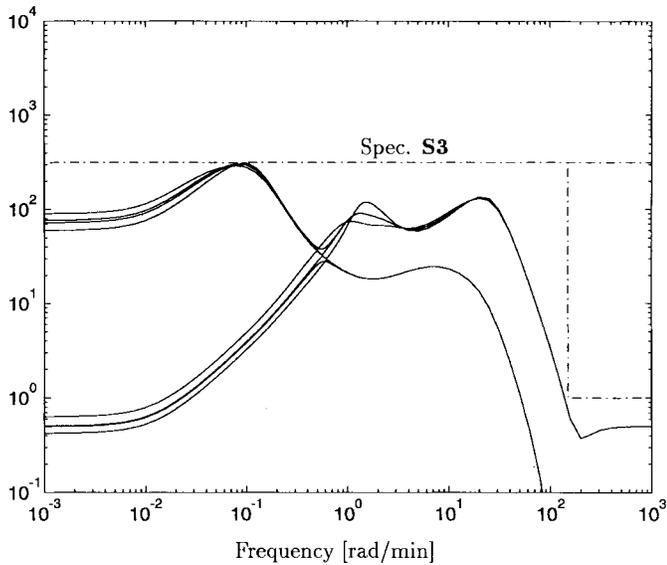


Fig. 14. Maximum and minimum singular values of $K_y \hat{S}$ for TDF-Alt.2 controller for four different plants.

but on the other hand the complexity of the control problem increases.

We decided to select $n = 3$ and $c = 5$. Following the procedure in Section V-C we selected W_u and W_n as follows:

$$W_u(s) = \frac{1}{M_{KS}} \left(\frac{M_{KS}^{1/n} s + 1}{\frac{\omega_0}{1} s + 1} \right)^{(n-1)} I_{2 \times 2} \quad (30)$$

$$W_n(s) = \frac{\tau_{cl} s + A}{\tau_{cl} s + M_T} \left(\frac{M_{KS}^{1/n} s + 1}{\frac{1}{c\omega_0} s + 1} \right) I_{2 \times 2}. \quad (31)$$

After a few iterations and parameter adjustments a controller which satisfies **S1**, **S2**, **S3**, and **S4** Alt.2 was obtained. The final weight parameters and D -scales are given in Table V.

TABLE V
FINAL WEIGHT PARAMETERS AND D -SCALES FOR DESIGN TDF-ALT.2

Weight parameters									
τ_{id}	ζ_{id}	τ_{cl}	A	M_S	M_T	M_{KS}	ω_0	c	n
8.0	0.71	9.5	10^{-4}	3.0	2.5	1000	200	5	3

TABLE VI
CONTROL PERFORMANCE FOR TDF-ALT.2 WITH GAIN UNCERTAINTY AND SECOND-ORDER PADÉ APPROXIMATION OF A 1-MIN DELAY. (SEE ALSO FIG. 13)

step ch.	gain unc.		set-point tracking			interaction	
	k_1	k_2	$t = 30$	max	$t = 100$	max	$t = 100$
1	1.2	1.2	1.063	1.082	0.991	0.036	0.008
1	1.2	0.8	0.976	1.013	0.990	0.464	-0.001
1	0.8	1.2	0.977	1.031	0.999	0.424	0.010
1	0.8	0.8	0.908	0.998	0.998	0.130	0.002
2	1.2	1.2	1.050	1.067	0.994	0.036	0.008
2	1.2	0.8	0.995	1.036	1.001	0.264	0.008
2	0.8	1.2	0.994	1.019	0.992	0.305	0.001
2	0.8	0.8	0.951	0.999	0.999	0.130	0.002

The controller yields a closed-loop \mathcal{H}_∞ -norm of 1.0 and has 34 states. The number of states was reduced to 22 using optimal Hankel norm approximation, without violating the control objectives. The performance of the 22 state controller is shown in Fig. 13. The simulation results are also summarized in Table VI and are seen to satisfy specification **S2**.

Fig. 14 shows that the maximum peak of $\bar{\sigma}(K_y \hat{S})$ is 313, which is less than 316 (50 dB), as required in **S3**, and the unit gain crossover frequency, $\bar{\sigma}(K_y \hat{S}) = 1$, is below 150 rad/min, as required in **S4** Alt.2.

We obtained this reduction in controller gain at high frequencies with almost no deterioration in performance. Compared to TDC-Alt.1 the peak value of $N_{12} = \hat{T}$ was reduced from 3.4 to 2.6 (which is an advantage), whereas the peak value of $N_{21} = (I + K_y \hat{G})^{-1} K_r$ increased from 420 to 435.

VI. DISCUSSION AND CONCLUSION

The inability to independently penalize separate elements of the closed-loop transfer function complicates the performance weight selection in the μ -framework. The Hadamard weighted approach [3] does not exhibit this problem and will therefore yield better performance with respect to the specifications in the CDC problem, **S1**–**S4**. However, for a practical engineering problem the transfer functions N_{12} and N_{21} in Fig. 10 are of importance, so it seems reasonable to include them in the control problem.

The paper has shown how a demanding design problem, involving parametric gain-delay uncertainty and a mixture of time domain and frequency domain performance specifications, can be reformulated and solved using the structured singular value framework. A two degree-of-freedom controller was needed to satisfy the specifications. The results, in terms of meeting the specifications, are comparable or better than those given in [10], [3], and [21].

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